Adiabatic Expansion ($\Delta Q = 0$)
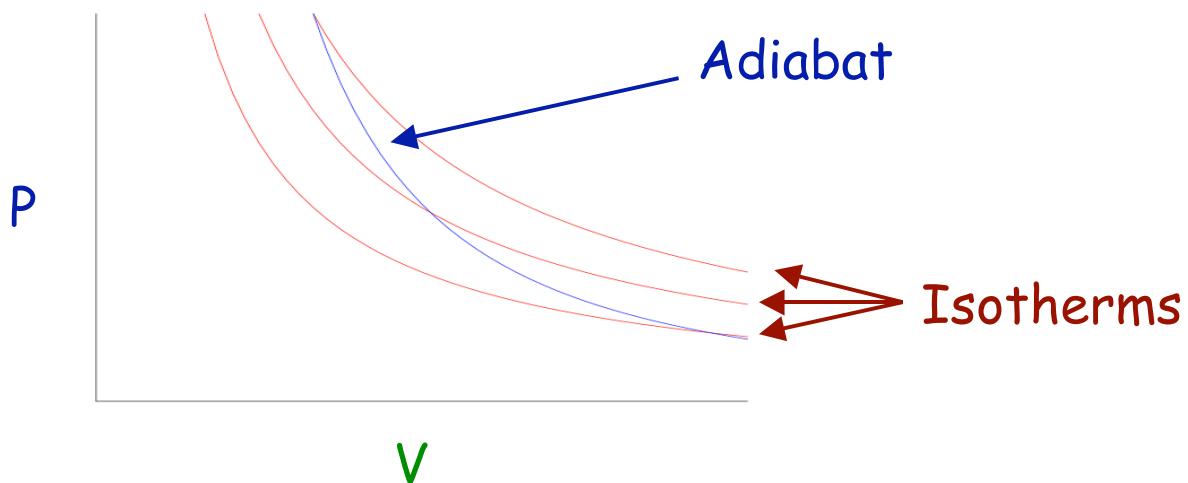
Occurs if:
- change is made sufficiently quickly
- and/or with good thermal isolation.

Governing formula:

$$PV^{\gamma} = \text{constant}$$

where $\gamma = C_P/C_V$

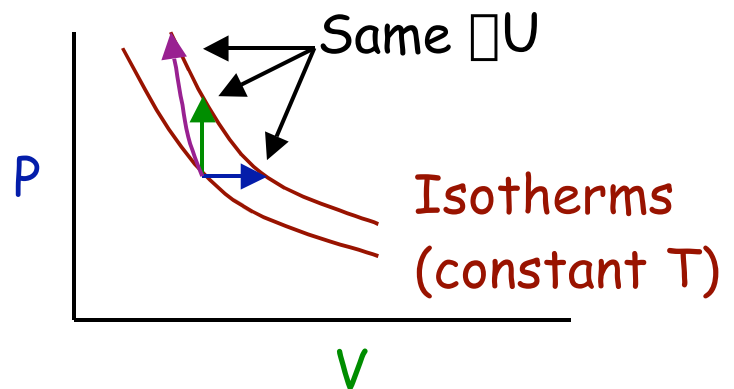Because PV/T is constant (ideal gas):

$$V^{\gamma-1} T = \text{constant} \quad \text{(for adiabatic)}$$

Proof of PV^{γ}=constant
(for adiabatic process)

1) Adiabatic: $dQ = 0 = dU + dW$
$$= dU + PdV$$

2) U only depends on T:

Same ΔU

Isotherms (constant T)

$dU = n\, C_V\, dT$ (derived for constant volume, but true in general)

3) Ideal gas: $T = PV/(nR)$
$$dT = [(dP)V + P(dV)]/(nR)$$

Plug into 2): $dU = (C_V/R)[VdP + PdV]$

Plug into 1): $0 = (C_V/R)[VdP + PdV] + PdV$

Rearrange:

$$(dP/P) = - (C_V+R)/C_V \, (dV/V)$$
$$= - \gamma \, (dV/V)$$

where $\gamma = (C_V+R)/C_V = C_P/C_V$

Integrate both sides:

$$\ln(P) = - \gamma \, \ln(V) + constant$$

or

$$\ln(PV^\gamma) = constant$$

or

$$PV^\gamma = constant$$

<u>QED</u>

Irreversible Processes

Examples:

  • Block sliding on table comes to rest due to friction: KE converted to heat.

  • Heat flows from hot object to cold object.

  • Air flows into an evacuated chamber.

Reverse process allowed by energy conservation, yet it does not occur.
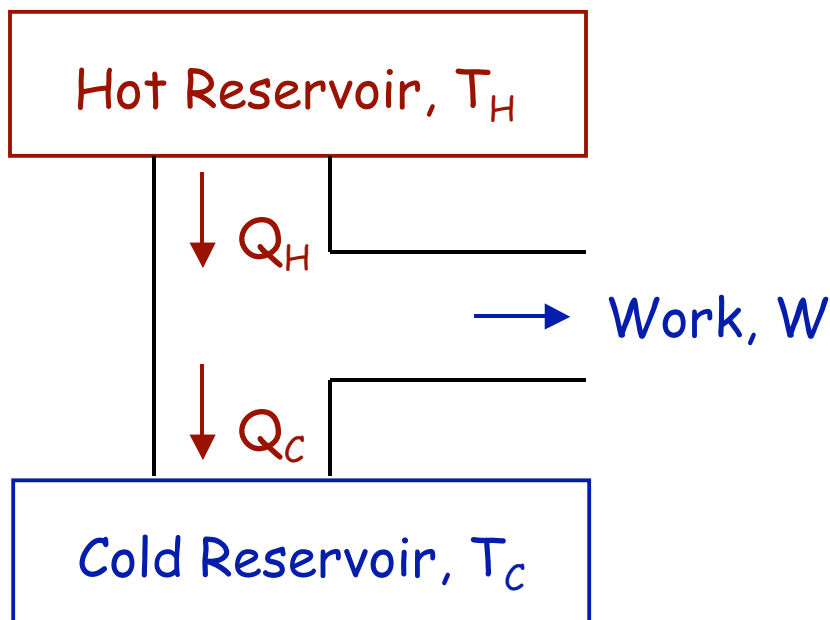
  ➡ arrow of time

Why?

2nd Law of Thermodynamics (entropy)

Heat Engines

Heat engine: a <u>cyclic</u> device designed to convert heat into work.

2<u>nd</u> Law of TD (Kelvin form):

It is impossible for a cyclic process to remove thermal energy from a system at a single temperature and convert it to mechanical work without changing the system or surroundings in some other way.

For a cyclic engine $\Delta U = 0$,

So work done is equal to
    heat in minus heat out:

$$W = Q_H - Q_C$$

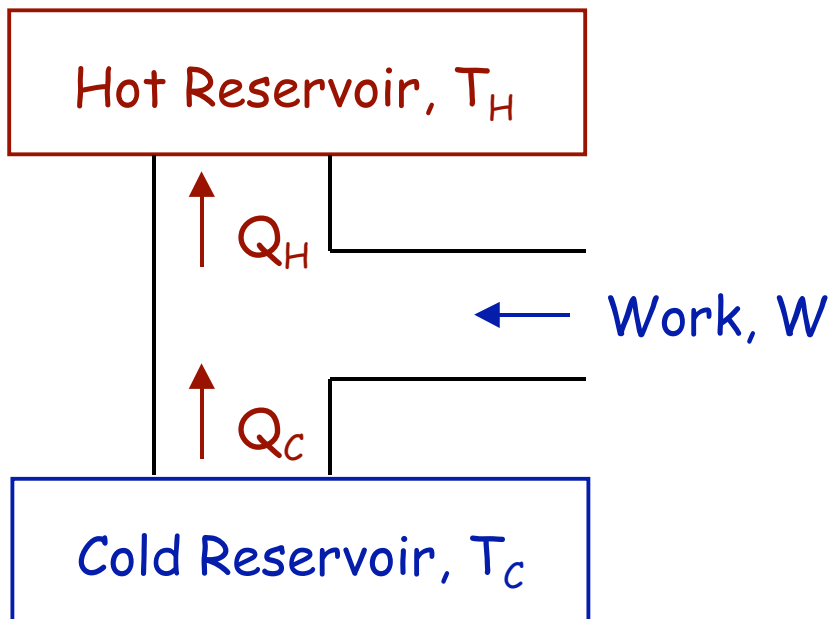Define the Efficiency of the engine:

$$\varepsilon = W/Q_H = (Q_H - Q_C)/Q_H = 1 - Q_C/Q_H$$

Corollary of the 2nd Law of TD:

It is impossible to make a heat engine whose efficiency is 100%.

Refrigerators

Refrigerator: a cyclic device which uses work to transfer heat from a cold reservoir to hot reservoir.

2nd Law of TD (Clausius form):

It is impossible for a cyclic process to have no other effect than to transfer thermal energy from a cold object to a hot object.

A measure of refrigerator performance is the ratio:

$$K = Q_C / W$$
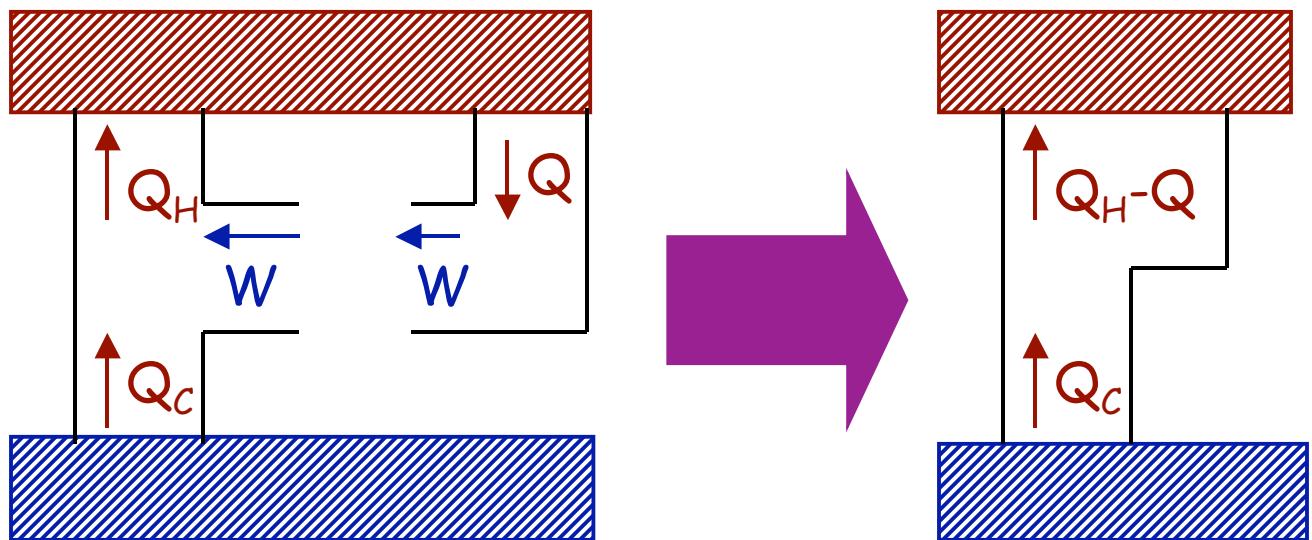
"Coefficient of performance"
(The larger the better.)

Corollary of the 2nd Law of TD:

It is impossible for the coefficient of performance to be infinite.

Equivalence of Kelvin and Clausius Statements

For example:

You could combine an ordinary refrigerator with a perfect engine (impossible)...

to obtain a perfect refrigerator (also impossible).

The Carnot Engine

2nd Law of TD says:
  100% efficient Heat Engine is impossible.

What is the maximum possible efficiency?

No engine working between 2 heat reservoirs can be more efficient than an ideal engine acting in a Carnot cycle.
(Sadi Carnot, 1824)

Properties of the Carnot cycle:

1. It is reversible: no friction or other dissipative forces.
2. Heat conduction only occurs isothermally at the temperatures of the two reservoirs.

Derivation of Carnot Efficiency
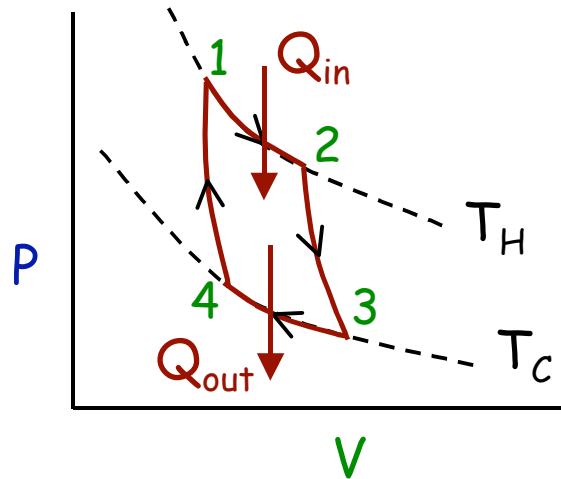
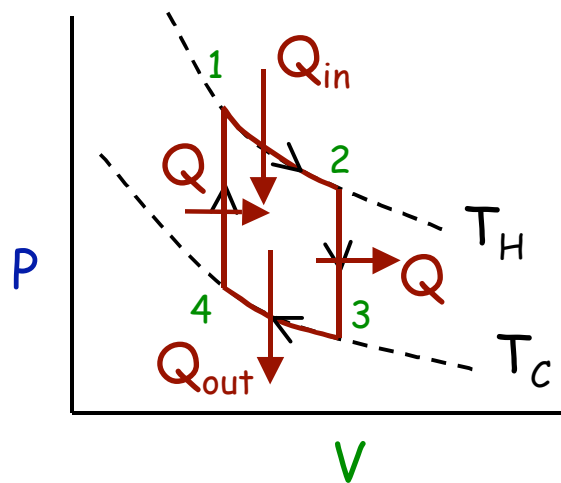1-2: Isothermal (Q_{in} at T_H)
2-3: Adiabatic expansion
3-4: Isothermal (Q_{out} at T_C)
4-1: Adiabatic compression

$$\varepsilon = 1 - T_C/T_H$$

The Stirling Engine

Invented by Robert Stirling in 1816.
Its operating cycle is:

The two temperature-changing steps are performed at constant volume; A heat transfer occurs at these steps also.

$$\varepsilon_{Stirling} < \varepsilon_{Carnot}$$

Entropy

Consider a reversible process for an ideal gas:

$$dQ = dU + dW = n \, C_V \, dT + P \, dV$$

$$= n \, C_V \, dT + n \, R \, T \, (dV/V)$$

We cannot write a general integral of this, because dW (and therefore dQ) depends on the functional form of T(V) (i.e. the path). However, if we divide by T:

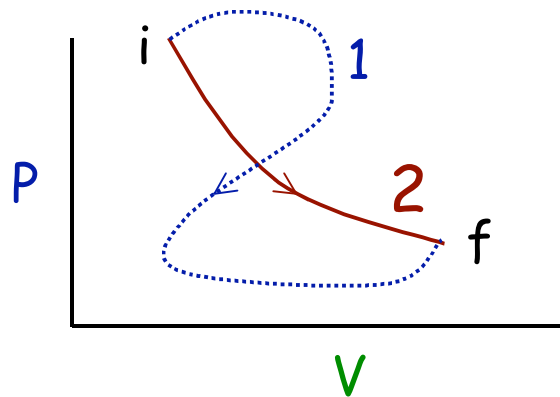$$dQ/T = n \, C_V \, (dT/T) + n \, R \, (dV/V)$$

is integrable independent of path.

This suggests a new <u>state function</u>, <u>Entropy</u>, defined by:

$$\Delta S = S_f - S_i = \int_i^f \frac{dQ}{T}$$

(Valid for any system)

In general, the process may be too complicated to do the integral (particularly if irreversible process):

However, because entropy is a state function, we can choose any convenient path between i and f to integrate.

For an ideal gas:

$$\Delta S = n\, C_V \ln(T_f/T_i) + n\, R\, \ln(V_f/V_i)$$

This only depends on the initial state (V_i, T_i) and final state (V_f, T_f), but not the path.

Isothermal Expansion: $T_f = T_i$, $V_f > V_i$

The amount of heat which leaves the reservoir and enters the gas is

$Q = n R T \ln(V_f/V_i)$.

The entropy change of the gas is

$\Delta S_{gas} = + Q/T = n R \ln(V_f/V_i)$.

The entropy change of the reservoir is

$\Delta S_{reservoir} = - Q/T$.

The net entropy change is

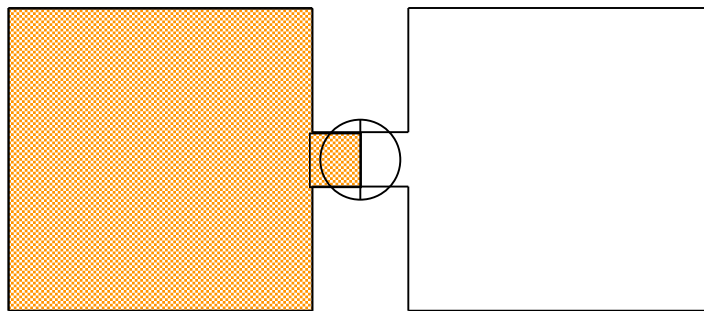$\Delta S_{universe} = \Delta S_{gas} + \Delta S_{reservoir} = 0$.

This illustrates a general result:

In a reversible process, the entropy change of the universe (system + surroundings) is zero.

Adiabatic Free Expansion of an Ideal Gas

Two containers connected by stopcock. They are thermally insulated so no heat can flow in or out.

Initial: One container is evacuated. Gas is in volume V_i at temperature T_i.
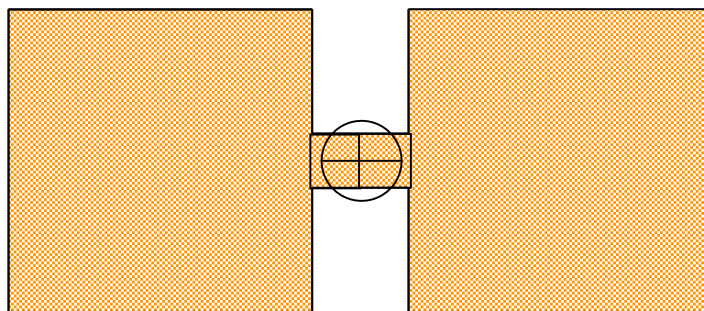
Final: Stopcock opened, gas rushes into second chamber. Gas does no work (nothing to push against) and there is no heat transfer. So internal energy does not change. Final volume $V_f > V_i$ at temperature $T_f = T_i$.

Because there is no heat transfer, you might think $\Delta S = 0$. WRONG! This is an irreversible process. We can't integrate

$$\int \frac{dQ}{T} \; .$$

But entropy is a state function, and we do know the initial and final conditions for the Free Expansion. They are exactly the same as for an Isothermal Expansion. So

$\Delta S_{gas} = n\,R\,\ln(V_f/V_i)$.

just as for an isothermal expansion. However, since it is thermally isolated from its surroundings,
$\Delta S_{surround} = 0$
and
$\Delta S_{universe} = \Delta S_{gas} + \Delta S_{surround} = n\,R\,\ln(V_f/V_i)$
> 0.

In an irreversible process, the entropy of the universe increases.

Entropy and Heat Engines

For a reversible cycle:

$$\Delta S = \oint \frac{dQ}{T} = 0$$

This implies that dQ cannot be strictly positive. There must also be heat released in the cycle.
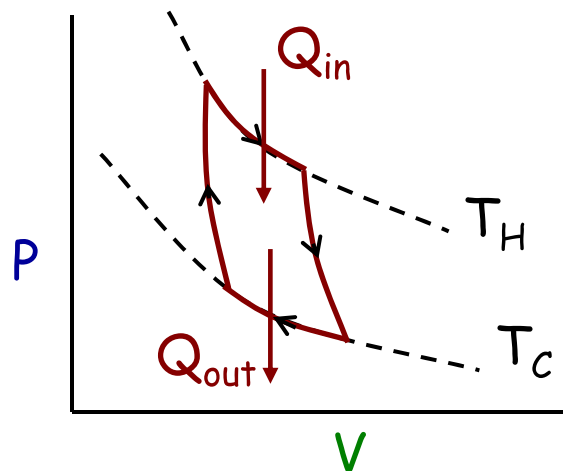
Carnot cycle: $(Q_{in}/T_H) + (-Q_{out}/T_C) = 0$.

2nd Law of TD (Entropy form):

$\Delta S_{universe} \geq 0$.

(greater-than sign for irreversible processes, and equals sign for reversible processes)

Entropy and Probability
(A statistical view)

Entropy ~ a measure of the disorder of a system.

A state of high order = low probability
A state of low order = high probability

In an irreversible process, the universe moves from a state of low probability to a state of higher probability.

We will illustrate the concepts by considering the free expansion of a gas from volume V_i to volume V_f.

The gas always expands to fill the available space. It never spontaneously compresses itself back into the original volume.

First, two definitions:

Microstate: a description of a system that specifies the properties (position and/or momentum, etc.) of each individual particle.

Macrostate: a more generalized description of the system; it can be in terms of macroscopic quantities, such as P and V, or it can be in terms of the number of particles whose properties fall within a given range.

In general, each macrostate contains a large number of microstates.

An example: Imagine a gas consisting of just 2 molecules. We want to consider whether the molecules are in the left or right half of the container.
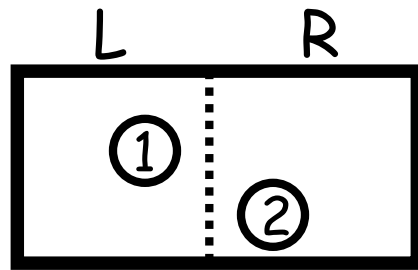
There are 3 macrostates: both molecules on the left, both on the right, and one on each side.
There are 4 microstates:
LL, RR, LR, RL.

How about 3 molecules? Now we have:
LLL, (LLR, LRL, RLL), (LRR, RLR, RRL), RRR
↑   ↑   ↑   ↑
(all L)   (2 L, 1 R)   (2 R, 1 L)   (all R)

i.e. 8 microstates, 4 macrostates

How about 4 molecules? Now there are
16 microstates and 5 macrostates

(all L) (3L, 1R) (2L, 2R) (1L, 3R) (all R)
↑   ↑   ↑   ↑   ↑

1   4   6   4   1
number of microstates

In general:

```
              1   1
           1    2   1
        1    3    3    1
     1    4    6    4    1
   1   5   10   10   5   1
 1   6   15   20  15   6   1
1 7  21  35   35  21  7  1
1 8 28 56  70 56 28 8 1
```

N	W (2)	M (2)
1	2	2
2	4	3
3	8	4
4	16	5
5	32	6
6	64	7
7	128	8
8	256	9

2^N $N+1$

This table was generated using the formula for # of permutations for picking n items from N total:

$$W_{N,n} = \frac{N!}{n!\,(N-n)!}$$

i.e. $W_{6,2} = \dfrac{6!}{2!\;4!} = 15$

"multiplicity"

<u>Fundamental Assumption of Statistical Mechanics</u>: All microstates are equally probable.

Thus, we can calculate the likelihood of finding a given arrangement of molecules in the container.

E.g. for 10 molecules:

Conclusion: Events such as the spontaneous compression of a gas (or spontaneous conduction of heat from a cold body to a hot body) are not impossible, but they are so improbable that they never occur.

"Improbable", quantitatively:

For large N, $\sigma/\mu \to 1/\sqrt{N}$

For N ~ N_A, $\sigma/\mu \to 1.3 \times 10^{-12}$

~ 70% of time within 10^{-10} % of expected

Probability of $< 10^{-99}$ to find more than 2.7×10^{-9} % from expected!

We can relate the # of microstates W of a system to its entropy S by considering the probability of a gas to spontaneously compress itself into a smaller volume.

If the original volume is V_i, then the probability of finding N molecules in a smaller volume V_f is

Probability $= W_f/W_i = (V_f/V_i)^N$

$\ln(W_f/W_i) = N \ln(V_f/V_i) = n N_A \ln(V_f/V_i)$ (1)

We have seen for a free expansion that

$\Delta S = n R \ln(V_f/V_i)$,

So, using (1) for $\ln(V_f/V_i)$,

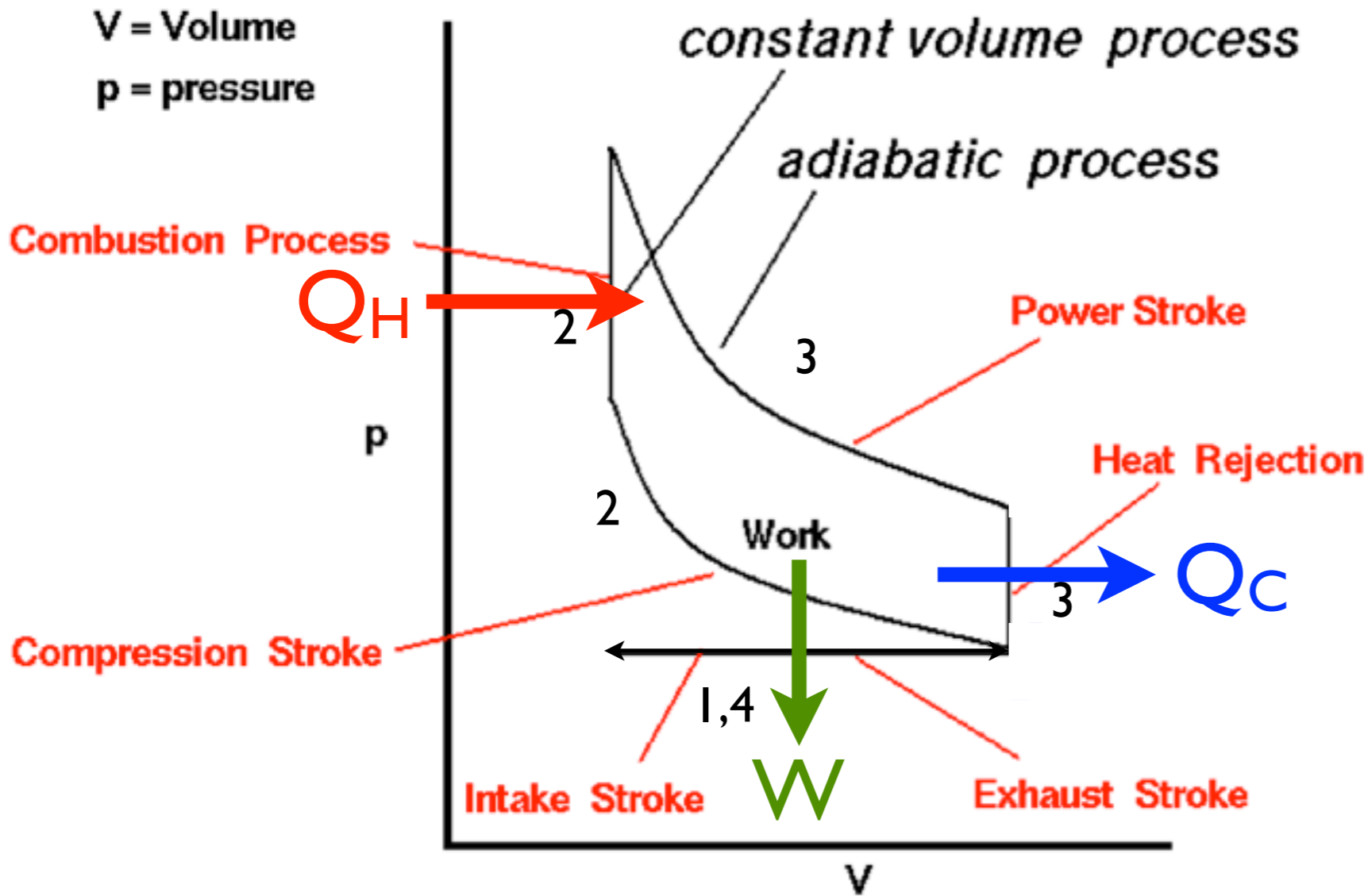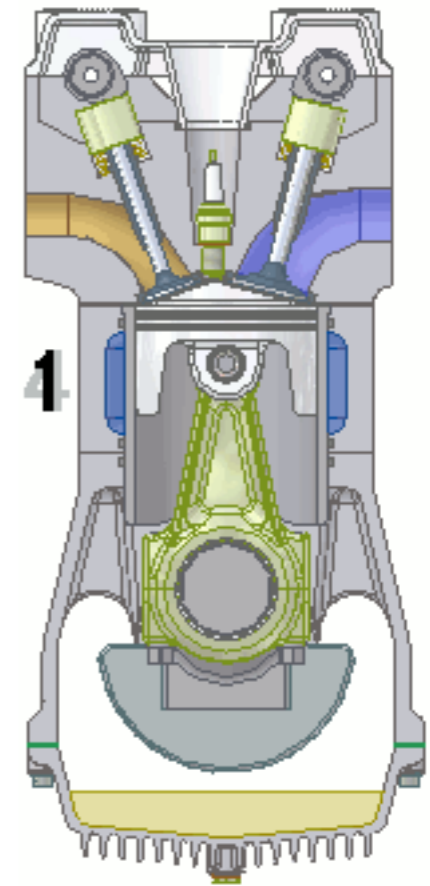$\Delta S = (R/N_A) \ln(W_f/W_i) = k_B \ln(W_f/W_i)$

or

$$S_f - S_i = k \ln(W_f) - k \ln(W_i)$$

Thus, we arrive at an equation, first deduced by Ludwig Boltzmann, relating the entropy of a system to the number of microstates:

$$S = k \ln(W)$$

He was so pleased with this relation that he asked for it to be engraved on his tombstone.

Otto Cycle

V = Volume
p = pressure

Q_H

constant volume process

adiabatic process

Combustion Process

2

3

Power Stroke

Heat Rejection

p

2

Work

Q_C

3

Compression Stroke

1,4

Intake Stroke

W

Exhaust Stroke

V

$$W = Q_H - Q_C$$

$$\eta = \frac{W}{Q_H}$$

Images: http://www.grc.nasa.gov & http://en.wikipedia.org

Ideal Gas Otto Cycle

V = Volume
p = pressure

constant volume process

adiabatic process

C

Combustion Process

Q_H

2

B

2

Power Stroke

3

D Heat Rejection

Work

Q_C

3

A

Compression Stroke

1,4

Intake Stroke

W

Exhaust Stroke

p

V

n moles of an ideal gas

$$W = Q_H - Q_C$$

$$Q_H = nC_V(T_C - T_B) \quad Q_C = nC_V(T_D - T_A)$$

$$\eta = \frac{W}{Q_H} = 1 - \frac{Q_H}{Q_C} = 1 - \frac{T_D - T_A}{T_C - T_B}$$

$$V_B = V_C \ \& \ V_A = V_D$$

$$T_B V_B^{\gamma-1} = T_A V_A^{\gamma-1} \ \& \ T_C V_B^{\gamma-1} = T_D V_A^{\gamma-1}$$

$$\therefore \ \frac{T_D - T_A}{T_C - T_B} = \left(\frac{V_B}{V_A}\right)^{\gamma-1} = \frac{T_A}{T_B} = \frac{T_D}{T_C}$$

Hottest: T_C

Coldest: T_A

$$\eta = 1 - \left(\frac{V_B}{V_A}\right)^{\gamma-1} = 1 - \frac{T_A}{T_B} = 1 - \frac{T_D}{T_C}$$

$< \eta_{Carnot}!$

Image: http://www.grc.nasa.gov

Details of Otto Cycle efficiency calculation:

Define the compression ratio $r = V_B / V_A$

$$\text{and} \quad x = r^{\gamma-1}$$

The boxed expressions (from adiabatic expansion) can be rewritten (dividing by $V_A^{\gamma-1}$) in terms of x as

$$x\, T_B = T_A \qquad \text{and} \qquad x\, T_C = T_D \qquad (1)$$

which leads to $\quad x = T_A/T_B = T_D/T_C$

Now consider $y = (T_D - T_A) / (T_C - T_B)$ **(from $\eta = 1 - y$)**

$$y = (x T_C - x T_B) / (T_C - T_B) = x \qquad (\text{use (1)})$$

Thus:

$$\eta = 1-y = 1-x = 1 - T_A/T_B = 1 - T_D/T_C$$

The last expression is easy to compare with the Carnot efficiency using only the two extreme temperatures (A coldest, C hottest):

$$\eta_C = 1 - T_A/T_C$$

So $\quad \eta < \eta_C \qquad$ **since $T_D > T_A$**